

## On the Application of Nanofluid in Minichannel for Heat Transfer and Fluid Flow Analysis

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### ABSTRACT

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Heat transfer and flow of fluids are processes that are prevalent in thermal engineering. They occur in many aspects of energy utilization and management. Rapid technological advances in electronic devices through reduction of sizes or simply miniaturization leads to the development of integrated circuits of ultra-large-scale magnitude (ULSIC) as new generation high-performance dense module, but with a consequence on increase power density and extremely intense heat flux which hampers on the long-term reliability and efficiency, as well as reduction of mean time between failure (MTBF) of electronic devices. Conventional fluids failed to provide required heat removal from high heat flux generating electronic devices and heat exchangers, due to their inherent low thermal conductivity. Nanofluid is an advance innovative thermal engineering fluid capable of providing outstanding heat transfer improvement than the conventional fluids, thus, increasing thermal system productivity and ensure energy sustainability. The Micro (MC) and minichannels (MiC) are the preferred state-of-the-art transport passage nowadays and are receiving much attention from researchers. They differ from conventional channels for having a hydraulic diameter in the range of 0.01 – 0.2 mm and 0.2 – 3 mm for micro and minichannels, respectively. In this paper, the various recent experimental and numerical works on utilizing nanofluids in minichannels are reviewed and summarized with emphasis on heat transfer enhancement mechanisms and techniques employed, achievement of thermal improvement, and various thermal engineering applications.

#### Keywords:

Nanofluid, Minichannel heat sink, convective heat transfer, pressure drop, aspect ratio

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## 1. Introduction

Nanofluid technology is regarded as one of the key emerging technologies that are presently attracting great research efforts in thermal engineering with the aim to provide improved working fluid for efficient thermal dissipation from high heat flux generating devices. Miniaturization which

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involves reduction of sizes of components without compromise on the heat transfer capability is gaining popularity in modern electronic devices and heat exchangers. Rapid technological advances in these areas are continuously pushing the boundaries of heat transfer enhancement, hence, there is a need for a dynamic, efficient and sustainable approaches toward heat transfer improvement through continuous research and development.

Tuckerman and Pearce [1] pioneered the use of micro (MC) and minichannels (MiC) in heat sinks which differ from the conventional channels in terms of channel hydraulic diameters. They postulated that reduction in channel hydraulic diameter can increase the heat transfer coefficient. The minichannel is usually within 200 $\mu$ m to 3mm hydraulic diameter based on Kandlikar and Grande classification scheme that distinguished the channels based on manufacturing restrictions and the Knudsen number [2]. Though microchannel offers higher heat transfer enhancement than minichannel, its smaller hydraulic diameter leads to increase pumping power and pressure drop, as well as high cost and more sophisticated manufacturing techniques [3], thus, minichannel still receive interest for utilization in heat exchangers and heat sinks, as well as in micro-electro-mechanical system devices. Numerous investigators have measured the thermo-physical properties of nanofluids through experiment [4, 5], whereas some employed well-known predictive correlations through analytical or numerical methods [6-11].

The mechanism that influences thermal and hydrodynamic properties of nanofluids were highlighted by some researchers [5, 12-15] and the common mechanisms observed include: Brownian diffusion/motion that induce migration of nanoparticles, temperature gradient induced particles migration (thermophoresis), solid-like nanolayer formation at the nanoparticles surface, clustering mechanism, and interaction of nanoparticles' surface with base fluid compounds. Buschman *et al.*, [16] observed that the convective heat transfer capability of nanofluid is not anomalous as reported by some researchers. They compiled experiments from five independent research teams studying convective heat transfer and flow of nanofluids in different passages and plate heat exchangers. The result shows that improvement in heat transfer by nanofluids is equivalent to the increase in its thermal conductivity as compared to the base fluid and independent on the concentration or material of nanoparticle.

Many researchers have shown remarkable achievement of nanofluids in their works, such as in heat exchangers [17-19], electronic cooling [20], thermo-electric generators (TEG) [21, 22], solar energy harvest [23], refrigeration and energy recovery [24, 25] and other applications. Some researchers compiled an extensive review of literature in relation to utilization of nanofluid in minichannel as a passive means of heat transfer enhancement [26-32]. It is the view of the authors of this work that, there are recent advances that need to be highlighted to avail researchers in the field with state-of-the-art techniques and methods for further research on heat dissipation in electronic micro-devices and heat exchangers in industries. The objective of this paper is to provide a systematic review of the works conducted with emphasis on the state-of-art techniques used and novel approaches employed in carrying out experimental and numerical works on thermal and flow analysis using nanofluid and minichannel.

## 2. Status of Thermal and Flow Analysis using Minichannel and Nanofluids

A comprehensive review of related works and expression of researches conducted in this area was conducted to have a better understanding of the concepts involved in the study of the hydrothermal analysis of nanofluids in minichannel thermal devices with emphasis on heat transfer enhancement mechanisms and techniques employed, and achievement of thermal improvement. First, a classification of nanofluid was discussed, then the techniques used in heat transfer

enhancement, as well as methods (either experimental or numerical) employed in the study, were overviewed.

## 2.1 Classification of Nanofluids

Nanofluids are normally produced by dispersing powdered nanoparticles (NP) into the base fluid in two distinct methods, these include one step and two methods. Various Nanoparticle materials used in nanofluids production include metals (Cu, Ag, Au), oxide ceramics ( $\text{Al}_2\text{O}_3$ , CuO), nitride ceramics (AlN, SiN), carbide ceramics (SiC, TiC), semiconductors ( $\text{TiO}_2$  and  $\text{SiO}_2$ ) and carbon-based (Carbon nanotubes and Graphene). In addition, a combination of two or more nanofluids provides a hybrid nanofluid, which shows a better enhancement than the individual nanofluids that formed it, though with increased viscosity which sometimes reduces the level of enhancement.

Most researchers observed that, nanofluid has higher surface to volume ratio than the base fluid, hence, adding nanoparticles (NPs) usually in size of 1 – 100 nm in a base fluid can considerably improve heat transfer rate and consequently enhanced convective heat transfer coefficient (HTC), however, with a drawback on pressure drop, which subsequently demands more pumping power of working fluid. Other important factors of consideration include long-term stability and agglomeration of nanoscale to macroscale particles, which may block and erode the minichannel surface. Nanofluid is usually produced either through a single step or two step methods. An extensive review was conducted on the synthesis and production of nanofluids [33].

### 2.1.1 Metallic nanofluid

Metallic nanoparticles can be dispersed into a carrier fluid to form an improved thermal fluid. Few researchers used metallic NPs such as Bahiraei and Heshmatian [34] dispersed spherical silver NP of 40 – 50 nm in water (Ag- $\text{H}_2\text{O}$ ) to evaluate hydrothermal characteristics and entropy generation of a biological nanofluid in a liquid block heat sink for cooling of an electronic processor. The result at a concentration of 1% and Reynolds number of 500, indicates a temperature reduction of  $2.21^\circ\text{C}$  for the NP against water. Investigation of corrugation effect on the flow and thermal characteristics of Au- $\text{H}_2\text{O}$  nanofluid in the wavy channel was conducted by [35] using concentrations of 0% - 5% and Re 250-1500. They highlighted that the use of a wavy channel with a  $90^\circ$  phase shift is not desirable to dissipate heat from the devices. Triangular channel gave better enhancement, then by sinusoidal at  $45^\circ$ ,  $90^\circ$ , and  $135^\circ$  phase shift.

Nikkam *et al.*, [36] conducted an experimental study through fabrication and characterization of spherical Silver NP of 25-29 nm to determine the relevance of base fluids (Deionised water, pure water, Ethylene Glycol and the mixture of water-EG) on thermophysical properties of the nanoparticle. Using concentration of 1%, 1.5% and 2wt.% and operating temperature of  $20^\circ\text{C}$ , they obtained a highest HTC enhancement of 12.4% with only 6.1% increase in viscosity observed for 2 wt% of Ag- $\text{H}_2\text{O}$ /EG nanofluid, which indicated the preference of this base-fluid above all other colloids in thermal performance.

In another work, Bahiraei and Heshmatian [37] used Silver-Graphene (Ag/HEG) to investigate the efficacy and entropy generation of a novel hybrid NF in three different liquid blocks made up of aluminum for CPU cooling with Re of 500, 750 & 1000. They observed that the novel distributor liquid block exhibited superior efficacy from both thermal performance and irreversibility rates. Moreover, nanofluid has a sharp advantage over pure water in the liquid block's cooling. Hence, the hybrid nanofluid has good potential for cooling improvement in electronics. Azwadi and Adamu [38] investigated the effect of Silver-Graphene (Ag/HEG) and Copper-oxide Graphene (CuO/HEG)

nanofluids in a circular channel under constant heat flux within turbulence regime using concentration of 0.4 – 1 vol%. and Re 10000 - 120000. At 1vol.%, enhancement of 34.34% and 38.72% were obtained for Ag/HEG at Reynold numbers of 60000 and 40000, respectively. similarly, 35.95% and 43.96% were obtained for CuO/HEG at the same Reynolds number and concentration respectively. Other researchers that employed metallic nanofluids in their works include Ag-HEG [39, 40] and Cu-H<sub>2</sub>O [41, 42].

### 2.1.2 Non-Metallic nanofluid

The commonest used nanoparticles are Alumina (Al<sub>2</sub>O<sub>3</sub>), Titania (TiO<sub>2</sub>) and Silica (SiO<sub>2</sub>), with Alumina as the most widely preferred by most of the researchers due to its lower density and viscosity as well as increased reactivity when compared with other conventional micron-sized particles. Stability and rheology of Alumina as nanoparticle was carried out by [43], while formulation of metal-oxide nanofluids and their thermo-physical properties, mechanisms, and heat transfer performance was reviewed by [44] and concluded that the interactions between metal oxide NPs and glycol resulted in reduced viscosity of nanofluids due to interfacial hydrogen bonding formation, and the lower the viscosity of the base fluids, the higher the thermal conductivity improvement due to Brownian motion induced convection.

Bahiraei and Heshmatian [45] investigated multi-objective optimization of energy efficiency of the liquid block for electronic cooling using Alumina nanofluid with variable sizes of 40 - 100 nm at volume fractions of 1 - 4 % and Re 400 - 1000. They observed that the nanofluid concentration and particle size effects on the surface temperature is larger than that on the pumping power, whereas the Reynolds number shows rather a similar effect on the two objective functions with optimum values found to be 666, while the concentration attained maximum value of 0.4% and the particle size has its minimum value of 40nm. Dominic et al. [46] used similar nanofluid of 40 nm particle size, volume fraction of 0.5% and 0.8% and at Re of 700 – 3300 to investigate heat transfer and pressure drop between wavy divergent and wavy cross-sections and reported that, in the laminar regime, the heat transfer performance of divergent wavy minichannels was 9% higher and the pressure drop was 30–38 % lesser than that of the wavy minichannels having constant cross-section. The performance factor of divergent wavy minichannels was 110–113 % for nanofluids compared to 115–126 % for water. Zhou *et al.*, [47] confirmed Alumina enhanced the heat transfer performance and the average saturated flow boiling HTC of specified concentrations of nanofluid respectively increased by 11.2%, 15.4% and 18.7% in comparison with deionized water.

TiO<sub>2</sub> (Anatase and Rutile) are two classes of Titania and were used by [48] to investigate steady-state laminar flow regime analysis for heat transfer performance of inline and staggered-pin fin heat sinks. The results show that TiO<sub>2</sub>(R)/H<sub>2</sub>O nanofluids exhibited 16.46% higher enhancement in contrast to 15.27% for TiO<sub>2</sub>(A)/H<sub>2</sub>O nanofluids in staggered and inline pin fin heat sinks. The minimum base temperature at a power of 192 W attained is 29.4°C using TiO<sub>2</sub>(R)/H<sub>2</sub>O nanofluid with staggered pin fin heat sink. Naphon and Nakharintr. [49] dispersed TiO<sub>2</sub> of 21 nm size in distilled water to analyzed heat transfer performance of nanofluid for cooling of MiCHS at Re 200. HTC for the heat sink with w=1.5 and 2mm averagely appreciates by more than 27% for the nanofluids in contrast to the de-ionized water of 42.3%. [50] investigated convective heat transfer characteristics of aqueous TiO<sub>2</sub> nanofluid under laminar flow conditions.

### 2.1.3 Hybrid and carbon nanotubes

Hybrid nanofluid and Carbon based nanorods and flakes like Carbon Nanotube (Single [51] and multi-walled CNT [52]) and Graphene are receiving interest from researchers. Bahiraei *et al.*, [53] studied thermal and hydraulic characteristics of a non-Newtonian hybrid nanofluid  $\text{Fe}_3\text{O}_4$  coated with Tetra Methyl Ammonium Hydroxide (TMAH) NPs and Carbon Nanotubes (CNTs) coated with Gum Arabic (GA) having concentrations of 0.1–0.9% and 0–1.35%, respectively. They confirmed adding NPs leads to further increment in heat transfer rate at lower Reynolds number compared with water, the nanofluid indicated heat transfer enhancement of 53.8% against 28.6% for water at Reynold numbers 500 and 2000 respectively. Shamsavari *et al.*, [54] used similar hybrid nanofluid but with different concentrations of 0.5–0.9% and 0.1–1.1%, respectively and found that increasing  $\text{Fe}_3\text{O}_4$  and CNT concentrations enhance the convective HTC of inner and outer walls and total entropy generation. Increasing radius ratio from 1/5 to 4/5, at CNT concentration of 1.1% and  $\text{Fe}_3\text{O}_4$  concentration of 0.7% led to decrease in the heat transfer coefficient of 85.05% and 35.49% for the inner wall and outer wall, respectively.

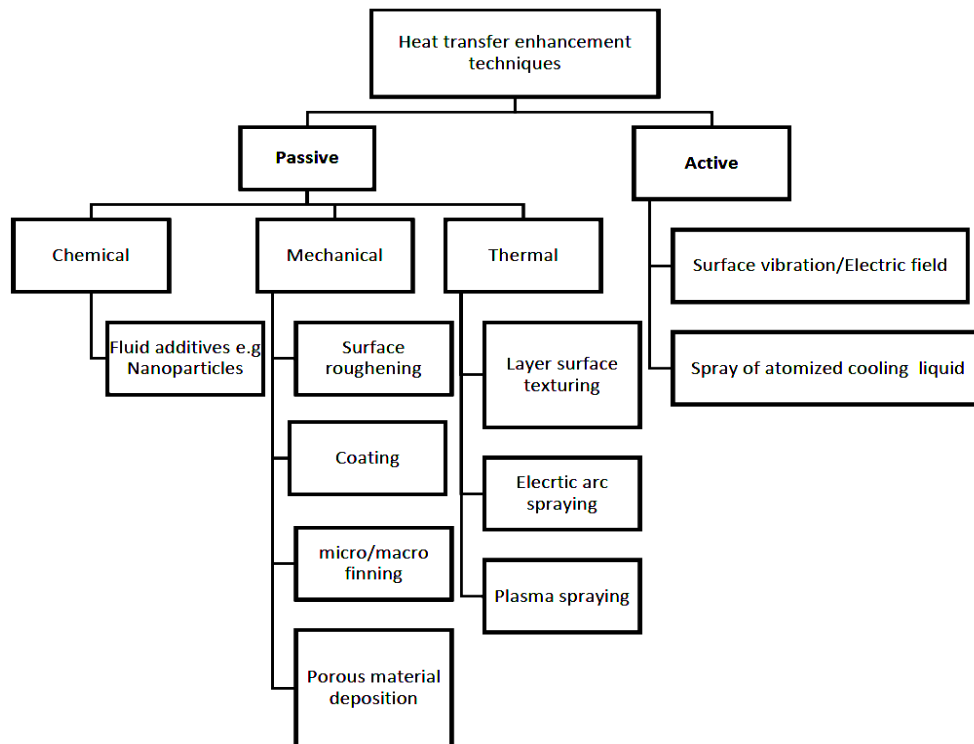
Diao *et al.*, [55] show that heat transfer improved with an increase in concentration at 0.01% or above but degenerated when concentration falls below 0.01% when they studied the thermo-hydraulic performance of Multi-walled CNT (MWCNT) passing through multi-port minichannel (MPMiC). The maximum PEC values of the MWCNT–water nanofluids at 0.01 vol.% for the smooth tubes, micro-fin (#1) and (#2) are 1.42, 1.37, and 1.32 at  $\text{Re} \approx 5200, 5300, \text{ and } 5300$ , respectively.

Microencapsulated Phase Change Material (MEPCM) is also gaining popularity recently among researchers and [56, 57] compiled extensive reviews on the application of nano and MEPCM in engineering applications. Ho *et al.*, [58] investigated the concurrent presence of hybrid nanofluid made of MEPCM and Alumina for thermal cooling of heat sink, they concluded that, use of hybrid nanofluid significantly improved the heat transfer in the heat sink, and the performance depends on Reynolds no, as pure nanofluid offer better result than hybrid nanofluid at high Reynolds no, hence adjusting  $\text{Re}$  and concentration of the hybrid nanofluid for a given heat flux can give superb thermal enhancement. In another work, [59] observed that heat dissipation depends on heat flow rates and NP showed 57% enhancement under the highest flow rate, whereas MEPCM showed averaged HTC of 51% under low flow rate, and in a similar work [60] they highlighted 52% heat transfer effectiveness has been achieved with the better improvement of thermal resistance obtained with lower flow rate. Other works that used Alumina include. [61-65].

A numerical research performed with different nanofluids to study their heat transfer and flow characteristics through circular minichannel heat sink for cooling was conducted by Soheli *et al.*, [66] using  $\text{Al}_2\text{O}_3$ -water,  $\text{CuO}$ -water,  $\text{Cu}$ -water and  $\text{Ag}$ -water at 0.5 vol.% to 4 vol.% and reported that, the highest HTC for  $\text{Ag}$ -water nanofluid was obtained at  $9718.96 \text{ W/m}^2\text{K}$ , which is 29.55% more in contrast to the pure water. In another work [67] analysed entropy generation as function of entropy generation ratio, thermal entropy generation and fluid friction of Copper (Cu), Alumina ( $\text{Al}_2\text{O}_3$ ) as the nanoparticle and  $\text{H}_2\text{O}$ , ethylene glycol (EG); reported that  $\text{Cu-H}_2\text{O}$  has 36% highest decreasing entropy generation ratio, which occurred at 6vol%.  $\text{Cu-H}_2\text{O}$  and  $\text{Cu-EG}$  nanofluid gave the maximum decreasing rates of the fluid friction entropy generation rate are 38% and 35% respectively at 6% volume fraction. It can be construed from the works discussed that, among the NPs, Cu has better enhancements, followed by  $\text{Al}_2\text{O}_3$  and  $\text{TiO}_2$  in terms of heat dissipation capability.

## 2.2 Heat transfer enhancement techniques

The mechanism used to enhance heat transfer without upsetting the overall thermo-hydraulic performance of the thermal system are simply categorized into active and passive methods. The later involves modifying properties and structure of the heating surface by increasing the effective surface area and residence time of the thermal fluid and has exhibited advance energy efficiency and material saving, hence its commonly used in heat transfer enhancement, while the former, demands some external power input for the heat transfer enhancement, due to energy conservation nowadays, it is rarely employed. Classifications of active and passive methods are depicted in Figure 1.



**Fig. 1.** Heat transfer enhancement techniques

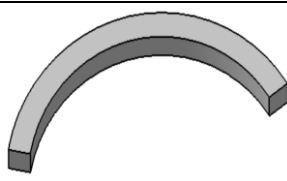
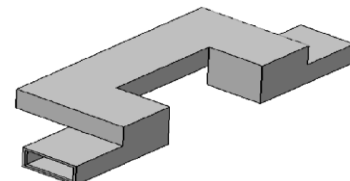
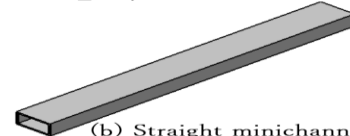
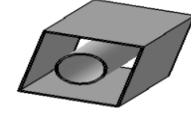
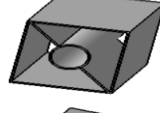
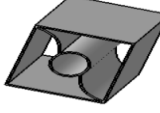
### 2.2.1 Active method

Few available types of research that employed active method include; Ozbey *et al.* [68] investigated the magnetic actuation of ferrofluid with dynamic magnetic fields in a small channel. Mohammadpourfard [69] investigated hydro-thermal behavior of magnetic nanofluid (ferrofluid)  $Fe_3O_4$ -kerosene and found that the Nusselt no is about 36% and 56% by applying the magnetic field in the peak point for an aspect ratio of 1 and 4, respectively. Naphon and Klangchart [70] studied numerically the effects of outlet port position on the heat transfer and flow on the jet liquid impingement characteristics in the mini-channel heat sink. They observed that the flow rate in each zone of the heat sink differs due to the velocity maldistribution and the positions of the outlet port have a substantial impact on the fluid flow through the entire heat sink and temperature distribution. Thus, in the thermal cooling of the heat sink, observing temperature non-uniformity is vital. Other researchers that employed active methods include [71-73].

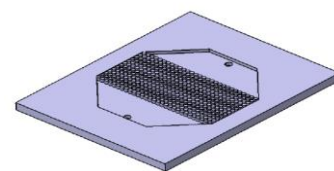
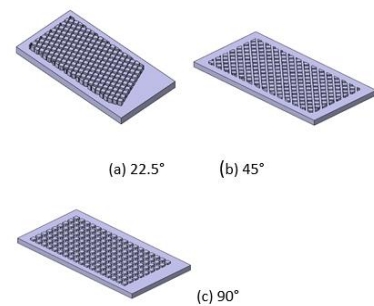
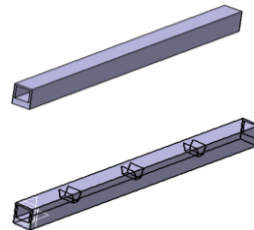
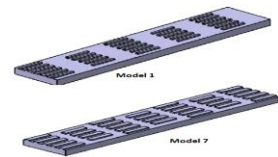
### 2.2.2 Passive method

Dominic *et al.*, [74] observed that passive method for forced convective heat transfer enhancement can be achieved through a decrease in thickness of thermal boundary layer, increase in fluid interruption and an increase in velocity gradient near a heat transfer wall. In addition, investigators observed that reduction of hydraulic diameter and higher heat transfer surface area per unit fluid volume of nanoparticles can effectively remove excess heat and improves heat transfer coefficient (HTC), thus, a lot of methods were introduced by changing minichannel geometrical parameters, such as channel number, aspect ratio, cross-sections, and path configurations. Table 1 illustrates some of the works that employed a passive method of heat transfer enhancement with a schematic representation of the minichannels used.

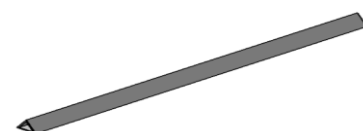
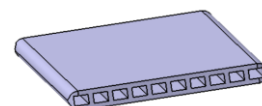
**Table 1**  
 Passive heat transfer enhancement technique using Nanofluid

Nanofluid system (NP/BF)	Passive technique	Principal remarks	Geometrical shape
Al <sub>2</sub> O <sub>3</sub> /H <sub>2</sub> O [75]	Chaotic flow	<ul style="list-style-type: none"> <li>Amongst the different shapes of particles, nanofluid with nanoplatelets show the largest convective heat transfer improvement and its followed by cylindrical, blade, spherical, and brick shaped NPs. The similar trend observed for pressure drop and convective HTC.</li> </ul>	
CMC/TiO <sub>2</sub> /H <sub>2</sub> O [76]	Chaotic flow	<ul style="list-style-type: none"> <li>Increased concentration and Reynolds number by 4% and 200 respectively, lead to frictional entropy generation increase, while thermal entropy generation decreases.</li> </ul>	 (a) C-shaped minichannel  (b) Straight minichannel
Al <sub>2</sub> O <sub>3</sub> /H <sub>2</sub> O [77]	Flow obstruction	<ul style="list-style-type: none"> <li>Thermal conductivity raises with a concentration of nanoparticles and these aggregated effects enhance convective HTC at Re 1000 and 5vol.% by 26.47% compared to water.</li> <li>Heat transfer enhancement of 84.4% and 199.6% for 1vol% and 5vol.% respectively, observed for nanofluid at Re=100.</li> </ul>	 (a) Minichannel with cylinder  (b) Minichannel with cylinder and fin  (c) Minichannel with cylinder and wavy fin

Al <sub>2</sub> O <sub>3</sub> -H <sub>2</sub> O [78]	Flow obstruction	<ul style="list-style-type: none"> <li>Enhancement in heat transfer observed for the OSPMHSs at the least values of the studied design parameters, i.e. <math>t = 1 \text{ mm}</math>, <math>\ell = 5 \text{ mm}</math>, <math>pt = 1 \text{ mm}</math>, and <math>pl = 5 \text{ mm}</math>.</li> </ul>
Al <sub>2</sub> O <sub>3</sub> -H <sub>2</sub> O and MWCNT-H <sub>2</sub> O [79]	Flow obstruction	<ul style="list-style-type: none"> <li>Al<sub>2</sub>O<sub>3</sub>-H<sub>2</sub>O nanofluid with 1 vol.% shows the highest overall performance in the triangular pin fin miniature channel, though MWCNT-water nanofluid gives the highest and least overall performance in the trapezoidal pin fin of type (3) and triangular pin fin, respectively.</li> </ul>
Graphene nanoplatelets [80]	Flow obstruction	<ul style="list-style-type: none"> <li>Amongst the three configurations, 22.5° heat sink has shown better enhancement as compared to other heat sinks and the average enhancements observed by 22.5°, 45°, and 90° heat sinks are 23.86%, 22.44%, and 19.68%, respectively.</li> </ul>
MWCNT [81]	Flow obstruction	<ul style="list-style-type: none"> <li>MWCNT bundle device exhibited 2.3 more heat flux removal from a silicon base than the other set up. And fully covered MWCNT device indicated 1.6 times the heat flux required to maintain the same silicon base temperature.</li> </ul>
TiO <sub>2</sub> -H <sub>2</sub> O [82]	Flow obstruction	<ul style="list-style-type: none"> <li>Increase in Nusselt number by up to 158% at about <math>Re = 3600</math> and the maximum PEC value reached 2.0 at <math>Re = 5150</math>.</li> </ul>
Al <sub>2</sub> O <sub>3</sub> , HEG and their hybrid [83]	Flow restriction	<ul style="list-style-type: none"> <li>The increase of <math>Re</math> from 200 to 1000 leads to a decrease of total entropy generation from 0.0361 W/K to 0.0184 W/K for the maximum applied heat flux of 25 kW/m<sup>2</sup>.</li> </ul>
Al <sub>2</sub> O <sub>3</sub> /H <sub>2</sub> O. [84]	Flow restriction	<ul style="list-style-type: none"> <li>HTC enhances averagely by 56% with an increase in <math>Re</math> from 100 to 500 at 5%. Increasing the Reynolds number from 100 to 300 and from 300 to 500 decreases the</li> </ul>



MMFT (a) 1 fin (b) 2 fins (c) 4 fins

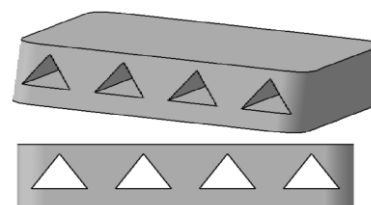




thermal entropy generation rate by 29.7% and 18.9%, respectively.

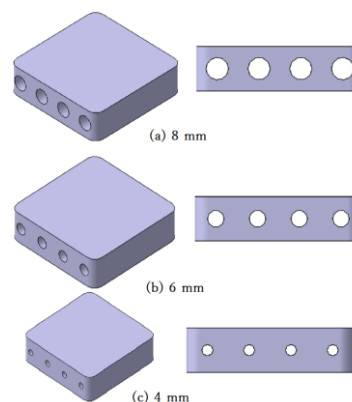
Al<sub>2</sub>O<sub>3</sub>-H<sub>2</sub>O [85] Flow restriction

- Thermal performance factor of 1.24 was obtained at Re 490 for 1.5 vol%, and at same Re, 1.12 and 1.07 were obtained at 1 vol% and 0.5 vol% respectively



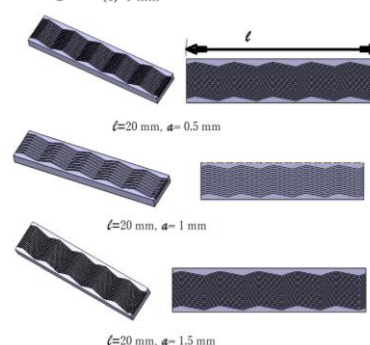
Al<sub>2</sub>O<sub>3</sub>-H<sub>2</sub>O [86] Flow restriction

- The increase of channel diameter reduces the pressure drop in the heat sink.
- The minichannel heat sink with a hydraulic diameter of 4 mm has a much lower thermal resistance than 6 mm and 8 mm.



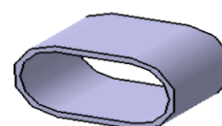
Al<sub>2</sub>O<sub>3</sub>-H<sub>2</sub>O [87] Flow restriction

- Using a CMCHS of 20 mm wavelength and 2 mm wave-amplitude, the lowest base temperature of 30.5°C at heater Power of 50 W.
- average performance factor of 2.68 obtained for the simultaneous utilization of corrugated minichannels and Al<sub>2</sub>O<sub>3</sub>/H<sub>2</sub>O nanofluid inside the MCHS.



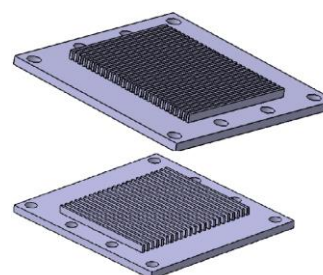
CuO/R600a-POE [88] Flow restriction

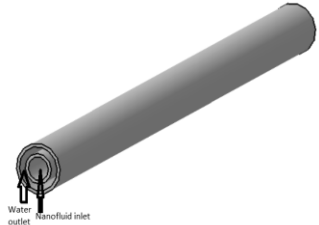
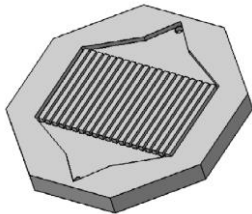
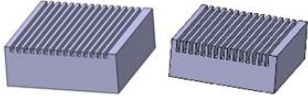
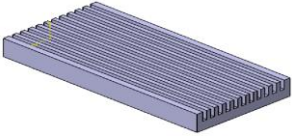
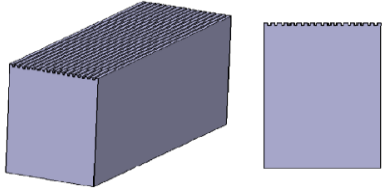
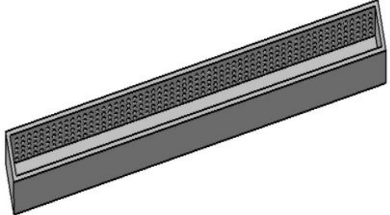
- Condensing HTC increased averagely by 4.1%, 8.11%, and 13.7% with respect to the R600a-oil mixture for the respective concentrations of 0.5%, 1% and 1.5%



MWCNT/DI H<sub>2</sub>O [89] Flow restriction

- the lowest base temperature of 49.7°C obtained at a heater power of 255W.
- The highest overall HTC recorded was 1498 W/m<sup>2</sup>K at a volumetric flow rate of 1 LPM for 0.2 mm fin spacing heat sink with MWCNT nanofluid coolant.
- Whereas, the lowest overall HTC was found as 1200 W/m<sup>2</sup>K at 0.5 LPM for 1.5 mm fin spacing heat sink with DI water as a coolant.



TMAH coated Fe <sub>3</sub> O <sub>4</sub> and GA coated CNTs [90]	Flow restriction	<ul style="list-style-type: none"> <li>increasing the Reynolds number, the minimum point of thermal entropy generation moves toward smaller magnetite concentrations. At low magnetite concentration, total entropy generation rate possesses a minimum (optimal) point with respect to CNT concentration while an ascending trend is observed at high magnetite concentrations.</li> </ul>	
Ag/H <sub>2</sub> O [34]	Straight channel	<ul style="list-style-type: none"> <li>Nanofluid's thermal conductivity improves with an increase in concentration and consequently, convective HTC enhances by 15.2% with increasing concentration from 0 to 1% at Re = 1500.</li> </ul>	
Al <sub>2</sub> O <sub>3</sub> /H <sub>2</sub> O [74]	Straight channel	<ul style="list-style-type: none"> <li>Nusselt number attained 76% maximum in the laminar region when Al<sub>2</sub>O<sub>3</sub>-H<sub>2</sub>O is used and 40% in the turbulent region in divergent straight MiC</li> </ul>	 (a) Straight MiC (b) Divergent MiC
Alumina and Titania [91]	Straight channel	<ul style="list-style-type: none"> <li>Alumina nanofluid indicated average HTC of 3.2% higher than that of water, while Titania has the same value as water. CFD simulation predicted a 5% HTC which is higher than that calculated from experimental readings.</li> </ul>	
TiO <sub>2</sub> -H <sub>2</sub> O [92]	Straight channel	<ul style="list-style-type: none"> <li>Using TiO<sub>2</sub> nanofluid, the lowest wall temperature is measured to be 37.05°C which occurred at Reynolds number of 922 and corresponding heating power of 100 W. Maximum enhancement of 12.75% for distilled water at 100 W</li> </ul>	
Al <sub>2</sub> O <sub>3</sub> -H <sub>2</sub> O [93]	Surface roughening	<ul style="list-style-type: none"> <li>Heat transfer and pressure drop were enhanced respectively by 3.73 times and 4.25 times as a function of (Xs/dp) and (Ys/dp) of 1.8.</li> </ul>	

### 2.3 Method of Heat Transfer Analysis

Heat transfer analysis like in other science and engineering fields employ experiments, numerical simulations and theoretical methods as tools to support research and development. The experimental method is more reliable, but factors such as speed, cost, repeatability, and safety, coupled with recent technological advancement and wide-spread access to computers make the simulation more preferred than experimental measurements or theoretical analysis. Some of the prospects and challenges of these methods were highlighted by [94, 95].

#### 2.3.1 Experimental heat transfer analysis

Ho *et al.* [96] investigated the thermal performance of Al<sub>2</sub>O<sub>3</sub>/H<sub>2</sub>O nanofluid with a weight fraction of 0.1–1 %. They varied the wall temperature between 50 °C and 110 °C and found that the nanofluid can enhance the heat transfer performance of the natural circulation loop studied and the average heat transfer effectiveness at the heating and cooling sections were approximately 3.5–22% and 9.5–62% respectively. Dominic *et al.*, [97] also employed Al<sub>2</sub>O<sub>3</sub>/H<sub>2</sub>O of 35 – 45 nm at volume fractions of 0.1%, 0.5% and 0.8 % with Re 700 – 1900 to investigate heat transfer and pressure drop for laminar flow in thermally developing and hydrodynamically developed regions and reported a contradictory result where the performance factor (PF) of water in wavy minichannels over their straight counterparts was higher than the nanofluids.

Arshad and Ali [98] investigated thermal and hydrodynamic performance of Graphene Nanoplatelets (GNP) in comparison to distilled water on integral fin heat sink and observed that the GNPs nanofluids indicated the lowest base temperature and maximum convective heat transfer enhancement as 36.81 °C and 23.91% coincide to Re 972 for heat flux of 47.96 KW/m<sup>2</sup>, respectively. Hussien *et al.*, [99] combined GNPs with MWCNT in water at low Re and low volume fraction and reported that heat transfer enhancement increases with an increase in nanoparticle concentrations, but decreases with increase in Reynolds no. The maximum enhancement obtained at 0.25% MWCNTs/0.035% GNPs hybrid and Re of 200 was 43.4%. Summary of other experimental works conducted in heat transfer analysis is presented in table 2.

**Table 2**

Summary of experimental investigations on heat enhancement of Nanofluids in minichannels

Nanofluid system (NP/BF)	Particle morphology (nm)	Nanofluid Concentration (%)	Validity range	Max. Heat improvement (%)	Principal findings
Ag/H <sub>2</sub> O (Silver-water) [100]	NA	0.25 to 0.5vol	Re 1000 - 100000	45.6	<ul style="list-style-type: none"> <li>increase in HTC with 0.5 vol% yielded 45.6% of the silver nanoparticles compared with that of the base fluid.</li> <li>HTC increased approximately by 12% in the laminar regime and 20–25% in the transition regime in relation to that of the base fluid.</li> <li>For higher Reynolds number above 10000 within the turbulent regime, the heat transfer coefficient is found to increase from 30 to 35%.</li> </ul>
Al <sub>2</sub> O <sub>3</sub> /H <sub>2</sub> O [101]	40 - 50	0.1 and 0.2 vol.	Re 200- 1000	40	<ul style="list-style-type: none"> <li>the COP of the thermoelectric module at 0.2 vol% shows 40% enhancement, but with reduction of 9.15% in the thermoelectric</li> </ul>

Al <sub>2</sub> O <sub>3</sub> /H <sub>2</sub> O [102]	20 & 80	0.41, 0.58, and 0.83	q= 285 - 1550 W/m <sup>2</sup>	-	<ul style="list-style-type: none"> <li>temperature difference between the hot and cold side.</li> <li>Local Nusselt number improved by 23.92% also at 0.2 vol.% in contrast with that of water at a Reynolds number of 1000 and at 400 W power input.</li> <li>Effectiveness of heat transfer is more in smaller particles for a fixed particle concentration, though increase in particle concentration results in some gains up to a certain threshold.</li> </ul>
Al <sub>2</sub> O <sub>3</sub> /H <sub>2</sub> O [103]	33	10wt	Re 133 -1515	57	<ul style="list-style-type: none"> <li>the largest enhancement of around 57% in 10wt% obtained at the highest flow rate of 1515.</li> </ul>
Al <sub>2</sub> O <sub>3</sub> /H <sub>2</sub> O [104]	40	5vol	Re 600 - 4500	19	<ul style="list-style-type: none"> <li>Thus, nanofluids should be utilized in either the laminar flow or fully developed turbulent flow at adequately high Re to yield enhanced heat transfer performance.</li> </ul>
Al <sub>2</sub> O <sub>3</sub> /H <sub>2</sub> O [105]	142 (max cluster)	0.1-0.25	Re 395 -989	18	<ul style="list-style-type: none"> <li>HTC enhanced by 18% and the heat sink base temperature (about 2.7 °C) was lowered by the nanofluid, however, it exhibited thermal resistance of 15.72% less at 0.25 vol.% and higher Reynolds number compared to the distilled water.</li> </ul>
Al <sub>2</sub> O <sub>3</sub> /H <sub>2</sub> O [106]	NA	0.05 to 0.2vol.	Vf 0.5 - 1.25 l/min	11	<ul style="list-style-type: none"> <li>11% reduction in entropy generation is recorded for the nanofluid compared with pure water. Density and frictional effects on the surface of the channel increases with the addition of nanoparticles</li> </ul>
Al <sub>2</sub> O <sub>3</sub> /H <sub>2</sub> O & TiO <sub>2</sub> /H <sub>2</sub> O [107]	NA	0.8, 1.6, 2.4, 3.2 and 4 vol.	NA	17.32	<ul style="list-style-type: none"> <li>thermal conductivity enhanced by 11.98% and 9.97% at 4vol% for Al<sub>2</sub>O<sub>3</sub> and TiO<sub>2</sub> dispersed in water respectively. Instead of water, Al<sub>2</sub>O<sub>3</sub>-H<sub>2</sub>O improves cooling up to 17.32%, similarly, TiO<sub>2</sub>-H<sub>2</sub>O achieved 1.88% to 16.53%.</li> </ul>
Al <sub>2</sub> O <sub>3</sub> /H <sub>2</sub> O [108]	25	1, 3, 5 and 7vol.	Re 40 - 1000	40	<ul style="list-style-type: none"> <li>40% heat transfer enhancement observed in the fully developed regime of the laminar flow.</li> </ul>
Al <sub>2</sub> O <sub>3</sub> /H <sub>2</sub> O & Al <sub>2</sub> O <sub>3</sub> -Polyalphaolefin (PAO) [109]	40	1, 2, 3.5 & 5 vol. (Al <sub>2</sub> O <sub>3</sub> /H <sub>2</sub> O) & 0.65 and 1.3 vol. (Al <sub>2</sub> O <sub>3</sub> -PAO)	Re 500 - 2500	-	<ul style="list-style-type: none"> <li>observed that the thermal efficiency of nanofluid is adversely offset by dual effects of increased viscosity and lower specific heat.</li> </ul>
Al <sub>2</sub> O <sub>3</sub> -Polyalphaolefin (PAO) [110]	60 (spherical) and 5 -11 (nanorod)	0.65 and 1.3vol	Re 350 and 490	28.70	<ul style="list-style-type: none"> <li>the enhancement in heat transfer efficiency of 28.7% at 1.3vol% was obtained for NF2 near the entrance, but it decreases below 21% as it approaches the channel exit.</li> </ul>
HEG/H <sub>2</sub> O [111]	-	0.05, 0.07, 0.10, 0.20 and 0.25 wt	-	21.55	<ul style="list-style-type: none"> <li>Found optimal conditions of concentration and flow rate of nanofluid at 0.1wt% and 950mL/min, at which 11.29%, 21.55% and 3.5% were recorded respectively for the improved voltage, output power and conversion efficiency.</li> </ul>
PCE [112]	290	10 and 20 wt.	Re 500 - 1000	-	<ul style="list-style-type: none"> <li>The heating power also affects the heat transfer performance of the PCE and the proposed correlation of heat transfer in laminar flow for the PCE shows a deviation</li> </ul>

						within $\pm 20.0\%$ compared to the experimental results.
SiC & Al <sub>2</sub> O <sub>3</sub> in H <sub>2</sub> O [113]	70 and 110 (Al <sub>2</sub> O <sub>3</sub> )	(SiC) 0.001, 0.005, 0.01, 0.1, and 1 vol.		85		<ul style="list-style-type: none"> <li>The friction factors at 1 vol.% increased by up to 39.2% and 51.6% for the SiC-water and Al<sub>2</sub>O<sub>3</sub>-water nanofluids, respectively.</li> <li>the SiC-water nanofluid Nusselt no surpasses the Al<sub>2</sub>O<sub>3</sub>-water nanofluid, with the maximum increases of 85% and 52%, respectively.</li> </ul>
SiC/H <sub>2</sub> O [114]	NA	0.001 to 0.1	Re 150 - 5200	80.85		<ul style="list-style-type: none"> <li>As the Reynolds number approaches 5200, the largest growth rate of Nusselt number runs up to 80.8% at a volume fraction of 0.01% compared with the results of base fluid.</li> <li>A smaller increase in resistance, along with the enhancement of heat transfer effect.</li> </ul>
SiO <sub>2</sub> , Al <sub>2</sub> O <sub>3</sub> , CuO/DI [115]	18.1, 28.3 and 45.6 H <sub>2</sub> O	0.25, 0.5, 1.0 and 2.0 vol.	Re 7000	40		<ul style="list-style-type: none"> <li>Heat transfer coefficient at 1 vol% was 40% higher than that of water at all Re. Also, at a fixed Re, a concentration of 2% of the nanofluid gives twice increase in heat exchange than with water</li> </ul>
SiO <sub>2</sub> & Al <sub>2</sub> O <sub>3</sub> [116]	10-100	0.5 to 2 vol.	-	-		<ul style="list-style-type: none"> <li>Inlet temperature found to be significant on turbulent heat transfer performance of nanofluids.</li> <li>Increase in nanoparticles concentration at fixed Reynolds number leads to the increase in local and average heat transfer coefficients.</li> </ul>
TiO <sub>2</sub> -H <sub>2</sub> O, Cu-H <sub>2</sub> O & SiO <sub>2</sub> -H <sub>2</sub> O [117]	NA	0.05, 0.01, 0.1, 0.5, and 1 vol.	Re 97 - 6200	43		<ul style="list-style-type: none"> <li>The Nusselt number increases with increasing volume concentration, then depreciate, paving the way to an optimal volume concentration. When Re reaches 6200, the Nusselt number increases by up to 43% for 0.01% TiO<sub>2</sub>-water nanofluid.</li> <li>TiO<sub>2</sub>-water nanofluids at 0.01% concentration displayed the superb performance.</li> </ul>
TiO <sub>2</sub> -H <sub>2</sub> O [118]	10, 30 and 50	0.005, 0.01, 0.1, 0.5 and 1 vol.	Re 100 - 6100	61		<ul style="list-style-type: none"> <li>TiO<sub>2</sub> with the size of 10 nm indicated an increase of 61% for the Nu at 0.01 vol.% and Re Of 6100. while maximum PEC obtained is 1.52 at the same parameters.</li> </ul>
ZnO/Al <sub>2</sub> O <sub>3</sub> [119]	24	0, 1, 2 and 4 wt.		29.7		<ul style="list-style-type: none"> <li>The highest heat enhancement of 44.6% in CHF and 29.7% in HTC have observed for the 4wt.% and mass flux of 88kg/m<sup>2</sup>s of surfactant added to ZnO-Al<sub>2</sub>O<sub>3</sub> composite coating. Thus, hydrophilicity increases with increase in doping level.</li> </ul>

### 2.3.2 Numerical simulation

Solutions of governing equations in numerical methods known as discretization normally involves a Finite Volume Method (FVM), Finite Element Method (FEM) and Finite Difference Method (FDM). The FVM and FEM methods are applicable to both structured and unstructured grids, while FDM uses only structured grids [120]. Mostly researchers in thermo-hydraulic analyses employ Finite

Volume Method (FVM). It is based on the integral form of governing equations and solves for the represented variable value for the cell volume, with control volume, a volume of fluid (VOF) and the mixture as common models. Some researchers have reported the application of different solution methods such as Inverse Heat conduction (IHC), Function Specification Method (FSM), Singular Value Decomposition (SFS) and Conjugated Gradient Method (CGM) [121, 122].

The governing equations used include that of mass, momentum, and energy for steady-state laminar incompressible fluid usually in non-dimensional form. The governing equations can be expressed either in polar or cartesian coordinates for cylindrical and channel geometries, respectively. The cartesian three-dimensional governing equations were given in equations 2 to 5 under section 3.1.2.

### 2.3.2.1 Single-phase

Some researchers considered nanofluid as a homogenous mixture and they used the single-phase model to study heat transfer performances of NP with various thermophysical parameters. Classical theories [123-127] were employed for the study, however, mostly these classical theories failed to adequately solve thermo-hydraulic properties, hence some researchers proposed some correlations [128, 129].

Pati *et al.*, [130] used the single-phase model to investigate the thermohydraulic performance of two different configurations of the sinusoidal wavy-walled channel formed by changing phase shift angles between the bi-opposite heated walls. They observed that heat transfer depends on the geometry of the wall and highly controlled by the wavelength of the wall waviness. For instance, the rate of heat transfer at the lower wavelength is almost same for both the channels, whereas for racoon channel is always more than that for the serpentine channel for higher wavelength and the variation is more obvious for larger values of amplitude of wall waviness and Reynolds number. Moraveji *et al.*, [131] modelled laminar forced convection on  $\text{Al}_2\text{O}_3$  nanofluid with size particles of 33 nm and concentrations of 0.5, 1 and 6 wt.% within Re of 130 - 1600 in mini-channel heat sink performed in CFD by four individual approaches (single phase, VOF, mixture, Eulerian) of FVM.

### 2.3.2.1 Two-phase

Mostly, works on nanofluid for heat transfer enhancements were numerically solved using two-phase models with available approaches such as Eulerian, Lagrangian, mixture and volume of fluid (VOF), with an accurate prediction of the models indicated by researchers [84, 132, 133]. Naphon and Nakharintr [134] studied laminar convective heat transfer of single and two-phase models in 3D using  $\text{TiO}_2\text{-H}_2\text{O}$  with PS 21 nm, VF 0.4 vol% and Re 80 – 200 in mini-rectangular fin heat sinks made of copper. The two-phase numerical model gave better enhancement than experimental single-phase results for all the Reynolds numbers. The maximum variations from the experimental data for the two-phase and single-phase models are 1.66% and 3.74%, respectively. Saeed and Kim [135] studied numerically the thermo-hydraulic performance of  $\text{Al}_2\text{O}_3\text{-H}_2\text{O}$  in mini-channel heat sinks with four different channel configurations using single-phase and two-phase models and observed that two-phase mixture model predicted results agreed closely with an experimental model while single phase numerical model has underpredicted values of convective HTC.

Arjun and Rakesh [136] studied forced convective heat transfer in porous pin fins in rectangular silicon minichannels using MWCNT,  $\text{Al}_2\text{O}_3/\text{H}_2\text{O}$ ,  $\text{CuO}/\text{H}_2\text{O}$  NFs. Porous pin fins show better overall heat transfer performances than in traditional solid pin fins. Increase in nanofluid volume concentration, raises pressure drops, while heat fluxes in porous pin fin channels increase and maximal overall heat transfer attained at 0.01% concentration. Nu improve by 6% with regards to

porosity and 88 % with respect to 0.01% Al<sub>2</sub>O<sub>3</sub>/H<sub>2</sub>O. Ghasemi *et al.* [137] studied the influence of heat sink with two variants cross-sectional shapes on the flow and heat transfer characteristics using CuO-H<sub>2</sub>O of 29 nm and observed that rectangular channel has lower thermal resistance compared to circular channel at the same Reynolds number 490 and cross-section area. In their other work [138], they used the Eulerian two-phase model to analyze laminar forced convection heat transfer of nanofluid using TiO<sub>2</sub>/H<sub>2</sub>O at Re 200 -500 and concluded that heat transfer enhancement increases with an increase in Re with the optimum performance evaluation criterion occurred in Re 490 and 0.75vol% was around 1.23. Summary of other numerical works in heat transfer analysis are presented in table 3.

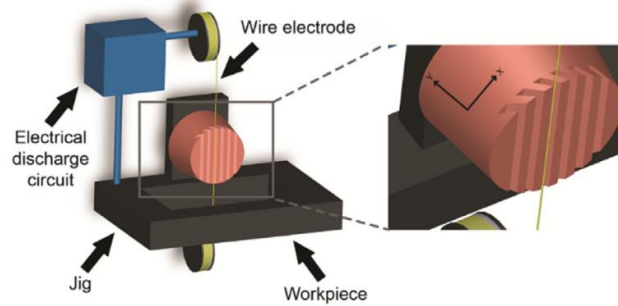
**Table 3**

Summary of numerical works on nanofluids in minichannel using single-phase models

Nanofluid system NP/BF	particle size (nm)	Concentration (%)	working parameter	Significant findings
TiO <sub>2</sub> /H <sub>2</sub> O [139]	20, 40, 60 & 80	1, 2, 3 & 4 vol.	Re 500-2000, q 10kW/m <sup>2</sup>	• The Bejan number higher than 0.8 at all concentrations, which signifies that heat transfer is responsible for more than 80% of the generated entropy.
Al <sub>2</sub> O <sub>3</sub> /H <sub>2</sub> O [140]	10, 50, and 90	1,3 and 5	Re 200, 1000 & 2000	• The rate of aggregate entropy generation diminishes by adding the nanoparticles to the water, which is advantageous in terms of energy utilization.
Graphene-PI [141]	NA	0, 0.02, 0.06 & 0.1 vol%	Re 331.7, 663.3, 995.0, 1326.7 and 1658.3.	• Higher heat transfer and pressure drop observed for the chaotic channel than the simple one. Significant improvement in heat transfer and minimal pressure drop noticed due to the superior qualities of Graphene. The figure of merit is always larger than 1.5 by using the chaotic channel instead of the simple channel.
CuO-H <sub>2</sub> O [142]	NA	0.02 - 0.04 vol%	Re 1000	• Convective heat transfer increases with the increase of inclination angle from 0° to 75°, while total entropy generation decreases.

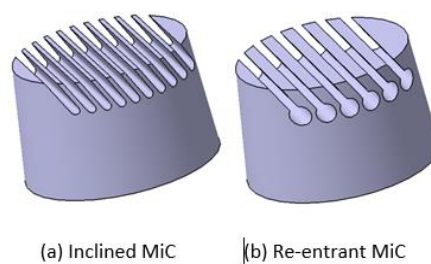
### 3. Manufacturing Techniques

Advanced technologies are employed in producing microscale channels. The most commonly employed technologies include micro milling using Computer Numerical control (CNC) machine, Electric discharge machine (EDM), Coating of metal-oxide on a substrate (such as in Sol-gel synthesis, thermal spraying, sintering, spray-pyrolysis), and using adhesive. Sujith *et al.*, [143] studied the effect of spray pyrolyzed Fe doped Al<sub>2</sub>O<sub>3</sub>-TiO<sub>2</sub> on critical heat flux using 0, 1.8, 3.6 and 7.2 % weight concentration of Fe. They found an overall enhancement of 52.39% and 44.11% in the CHF and HTC respectively, for 7.2% Fe doped TiO<sub>2</sub>-Al<sub>2</sub>O<sub>3</sub> for a mass flux of 88 kg/m<sup>2</sup>s. EDM process involves removal of electrically conductive material without physical contact with the electrode through localized melting/evaporation caused by electrical discharging, thus, it allowed minichannels fabrication on hard, brittle and refractory materials. Naphon and Nakharintr [144] fabricated minichannel heat sink from the copper by the wire EDM with the length, width and a fin height of 110, 60 and 1 mm, respectively. The Schematic of EDM process is shown in Figure 2.



**Fig. 2.** Schematic process of fabrication of inclined minichannel using EDM [145]

Pool boiling and flow boiling are thermal phenomena and their enhancement using nanofluids were comprehensively reviewed by Liang [146] and Das [147] respectively. Techniques to enhance heat transfer surface for flow boiling in a minichannel and pool boiling studies were reported by vibration-assisted laser and electro-machining [148], and by using laser and spark erosion [149, 150]. Akbari *et al.*, [151] studied the effect of inclined and re-entrant inclined minichannel on pool boiling enhancement through bubble dynamics of Ag-DZ-Nanocoolant shown in Figure 3. They observed that increasing nanoparticles concentration can increase the Critical Heat Flux (CHF) and Heat Transfer Coefficient (HTC) on the nano-coated surface by 120% and 100% higher than those of the plain surface. Gheitaghy *et al.*, [145] carried out similar work but by varying inclination and spacing of MiCs. Heat dissipation improved with an increase in channel inclination and depth, but with a decrease in channel pitch. The highest HTC and CHF up to 170% and 65% respectively were obtained for the orthogonally intersected minichannels compared to the plain surface. This improvement may be linked to bubble dynamics, heat transfer area, bubble slide and scrape, and capillary flow. They confirmed that EDM provides a more practical method of fabrication of inclined minichannels.



**Fig. 3.** Inclined and re-entrant minichannels configuration

## 4.0 Potential Engineering Applications of Nanofluids in Minichannels

### 4.1 Heat Exchanger

Heat exchangers are going through a transformation and the recent desire is to have lightweight, compact and more efficient heat exchangers for thermal management. Some researchers [2, 26, 152] have extensively reviewed the prospect of using minichannel in heat exchangers for fluid flow and heat transfer. Zewede *et al.*, [153] investigated the convective heat transfer of Ethanol/Polyalphaolefin(PAO) nanoemulsion flowing through a heat exchanger made of 12 circular MiC and reported 75% enhancement, while Trinh and Xu [154] used the same nanofluid reported increase in average Nusselt no of 24% and 11 % for 8 wt% and 4 wt%, respectively for nanoemulsion fluid compared to that of pure PAO at the same Reynolds number of 3400.



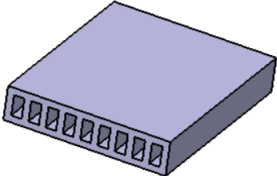
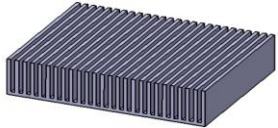
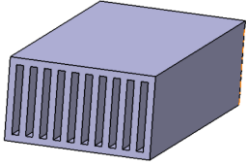
Sarafraz and Hormozi [155] observed heat transfer, pressure drop and fouling studies of multi-walled carbon nanotube nano-fluids inside a plate heat exchanger using inlet temperature between 50-70°C and Re 2500, and reported that increase in concentration and flow rate of nanofluid can enhance HTC. Under the same condition, the pressure drop increased. A non-linear prolong fouling behavior for nanofluid also observed. Ray et al. [156] compare the performance of three different nanofluids (Al<sub>2</sub>O<sub>3</sub>, CuO<sub>2</sub>, SiO<sub>2</sub>-ETG-H<sub>2</sub>O) in the compact heat exchanger and reported that among the nanofluid, aluminum oxide nanofluid of 0.5 vol% indicated enhanced convective and overall HTC of 11% and 4.85%, respectively.

#### 4.2 Electronic Cooling

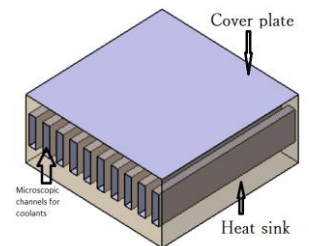
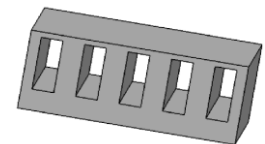
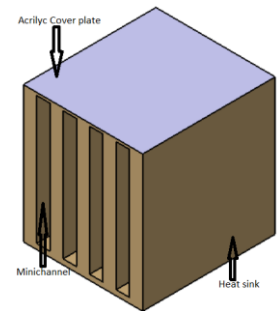
Heat sinks are regarded as a type of heat exchangers employed in electronic devices cooling, due to the simplicity of fabrication, low cost, and reliability of heat dissipation. They have extended surfaces which are either flat-plate fins or pins fins shapes [157]. Mostly investigators prefer using a liquid block with variable aspect ratio and number channels for electronic thermal management. Ma et al., [158] studied flow and heat transfer of a closed-loop cooling system for electronic thermal management using minichannel through power input of 0 - 240W with an increment of 20W each step. They reported that the system has a cooling capability of 240W (corresponding to a heat flux of 30 W/cm<sup>2</sup>) at the base temperature under 80°C. For efficient cooling of the heat sink in electronic devices, increasing surface area by an increase of aspect ratio can reduce the thermal resistance, hence, optimal design of the microscale channel is vital for reliable and practical performance.

Though, most of the investigators used single layer heat sink, however Karunanithi et al., [159] used a stacked multilayer of porous media, where the porosity varies from one layer to the next layer (porosity scaling) along with the heat transfer direction and indicated advantages over traditional single-layered channels in terms of both pressure drop and thermal resistance, but its inconvenient in terms of miniaturization and fluid volume. Summary of other work in cooling electronic devices using nanofluid and minichannel are presented in table 4.

**Table 4**  
 Liquid cooling blocks for Electronic devices heat sinks

Researcher	Nanofluid	Working Temperature (°C)	Power density (W/cm <sup>2</sup> )	Principal findings	Geometry
Kumar and Sarkar. [160]	Al <sub>2</sub> O <sub>3</sub> -H <sub>2</sub> O and Al <sub>2</sub> O <sub>3</sub> -MWCNT	27	8.3	Maximum HTC enhancement at 0.01vol% of hybrid nanofluids and minichannel depth of 0.5mm found as 15.6%, with insignificant pressure drop increment.	
Moraveji [161]	TiO <sub>2</sub> and SiC /H <sub>2</sub> O	NA	-	Increase in nanoparticles concentration and Reynolds number leads to higher heat transfer coefficient.	
Ijam et al. [162]	SiC/H <sub>2</sub> O and TiO <sub>2</sub> /H <sub>2</sub> O	35	12.44	thermal conductivity at 4 vol% of nanoparticles SiC/H <sub>2</sub> O and TiO <sub>2</sub> /H <sub>2</sub> O enhanced by 12.44% and 9.99% respectively. The nanofluids indicated thermal	

				efficiency of 7.25%-12.43%, and 7.73%-12.77% for SiC/H <sub>2</sub> O and TiO <sub>2</sub> /H <sub>2</sub> O respectively.
Khaleduzzaman et al. [163]	Al <sub>2</sub> O <sub>3</sub> /H <sub>2</sub> O (13 nm spherical)	NA	NA	Overall energy efficiency of 94.68%. indicated by Al <sub>2</sub> O <sub>3</sub> nanofluid with 0.25vol.% the highest improvement of outlet exergy of 60.86% of the heat sink at the same concentration compared to water at the flow rate of 1.0l/min.
Bergman. [164]	Al <sub>2</sub> O <sub>3</sub> /H <sub>2</sub> O (36 nm spherical)	35	NA	Found minimal enhancement and suggested limited usefulness of nanofluid in a heat sink cooling application.
Tuckerman & Pierson	Conventional fluid	71	790	maximum thermal resistances at downstream was around 0.1°C/W.cm <sup>2</sup> , and tested up to 790 W/cm <sup>2</sup> .



### 4.3 Solar

Mahian *et al.*, [165] evaluated the turbulent flow effect on the performance of minichannel-based solar collector using variety nanofluid (Cu/water, Al<sub>2</sub>O<sub>3</sub>/water, TiO<sub>2</sub>/water, and SiO<sub>2</sub>/water) having same size of 25 nm at 4vol% and indicated that amongst the nanofluids, Al<sub>2</sub>O<sub>3</sub>-H<sub>2</sub>O and Si<sub>2</sub>O<sub>3</sub>-H<sub>2</sub>O have the highest and lowest HTC respectively, whereas Cu-H<sub>2</sub>O has the lowest entropy generation. They further proposed a model to compute thermal conductivity based on consideration of aggregation and Brownian motion effect in the nanoparticles, it is expressed in equation (1)

$$\frac{K_{nf}}{K_f} = \frac{K_p + 2K_f - 2\phi(K_f - K_p)}{K_p + 2K_f + \phi(K_f - K_p)} + \frac{\phi\rho C_{pf}}{2K_f} \sqrt{\frac{2K_b T_{ave}}{3\pi d_p \mu_f}} \quad (1)$$

where, bf and np refer to base fluid and nanofluid, respectively. for nanofluid and hybrid nanofluid, np is 1 and 2, respectively.

While in another work [166], they examined the effects of nanoparticle shape and tube materials using First and second laws in a minichannel-based solar collector using boehmite alumina nanofluids. The heat exchanger is made up of copper and steel tubes. The result shows that steel tubes at a mass flow rate of 0.5 kg/s show an average entropy generation rate of 11% higher than copper tubes, while it reaches 18% for a mass flow rate of 0.75 kg/s. Sharaf and Orhan [167] used Al<sub>2</sub>O<sub>3</sub>/H<sub>2</sub>O (low to moderate temperatures) and Al<sub>2</sub>O<sub>3</sub>/synthetic oil (moderate to high temperatures) to analyze and optimize through Genetic Algorithm, densely packed receiver assembly components in high-concentration CPVT solar collectors. Suganthi et al. [168] investigated the heat transfer performance of the ZnO of 25 and 45 nm sizes and Propylene Glycol (PG), respectively in water for

solar energy collection & discharging of thermal energy storage. The nanofluids show a 16.5% rise in heat transfer rate for 2 vol% nanofluids at constant heat flux conditions. At the same concentration, the HTC on the coolant side increased by 29% for heat removal from a constant temperature source.

Three different aqueous nanofluids;  $\text{Al}_2\text{O}_3$ , CuO, and SiC were exploited in cooling of photovoltaic (PV) thermal units to enhance its efficiency due to increases in cell temperature obtained during conversion of a small part of the absorbed solar radiation into electricity with the remaining part been lost as heat. SiC shows the best stability and the highest thermal conductivity (4.8% at 4% concentration) compared to the other two nano-substances, while, CuO gave higher thermal conductivity than  $\text{Al}_2\text{O}_3$  but with lower stability, though it was observed that this material reliably stable compared to in other studies [169]. In overall, the nanofluid reduced the indoor PV/T system temperature and improved power generated.

#### 4.4 Refrigeration and other Specialized Cooling

Zhou *et al.*, [170] studied the impact of NP concentration on flow boiling heat transfer coefficients of nano-refrigerant in a micro heat exchanger by direct metal laser sintering. The particle size of the  $\text{Al}_2\text{O}_3$  was 96 nm. They concluded that the HTCs increased comparatively with the pure refrigerant R141b by 55.0%, 72.0%, 53.0%, 42.3% and 39.9% for 0.05, 0.1, 0.2, 0.3 and 0.4 weight% of  $\text{Al}_2\text{O}_3/\text{R141b}+\text{Span-80}$  nano-refrigerant, respectively. Hemmat *et al.*, [171] predicted and optimized the thermal and rheological characteristics of  $\text{Al}_2\text{O}_3/\text{antifreeze}$  using response surface methodology. Good agreement between the predicted and experimental values was observed. Thus, >99% of variations in viscosity and thermal conductivity of the nanofluid could be predicted by the models. Carbon nanofiber in ethylene and PVP were used as Nanocoolant at 0.1%- 1wt% and the presence of nanoparticles enhanced the forced convective heat transfer performance of the CNF-based nanofluid in a laminar flow as against the base fluid only, and the highest thermal conductivity of 0.642 W/m.K was obtained at volume concentration of 0.5 wt% and temperature of 40°C. [172, 173] also exploit the advantages of nanofluid in refrigeration systems.

Zakaria *et al.*, [174] analyzed thermal improvement for a single Proton Exchange Membrane Fuel Cell (PEMFC) cooling plate by a numerical method using low concentration  $\text{Al}_2\text{O}_3\text{-H}_2\text{O-EG}$ . The thermal performance improved by 7.3% and 4.6% for 0.5 and 0.1 vol % of  $\text{Al}_2\text{O}_3$  consecutively as compared to the base fluid of 50:50 (water: EG). Better heat transfer enhancement observed at a higher volume fraction of  $\text{Al}_2\text{O}_3$ , but with a penalty of higher pumping power required as much as 0.04W due to raising in pressure drop. Huang [175] viewed the use of effective cooling techniques as vital in high heat flux applications, such as aircraft combustion chambers. Regenerative cooling system, where coolant (e.g., engine fuel) flows through the cooling tubes along the chamber wall to dispel heat by forced convection and thermal cracking.  $\text{Al}_2\text{O}_3\text{-kerosene}$  nanofluids were discharged through a vertical upward mini tube at supercritical pressures. As the concentration of NPs increases, the HTC decreases due to the modification of the inner wall surface by the NPs.

#### 4.5 Biomedical systems

Sesen *et al.*, [176] uses  $\text{Fe}_2\text{O}_3$  with particle diameter of 32-100 nm to investigate microflows through electromagnetically actuation device and found that the magnetically actuated pump can achieve flow rates as high as  $\sim 30 \mu\text{l}/\text{min}$  with consumed power of 20 Watts and the flow rate can be controlled precisely down to  $\sim 5 \mu\text{L}/\text{min}$  with the micropump device, hence, this precise flow control device can be very useful in drug delivery systems. However, safety and production cost hamper the commercialization of this innovation.

## 5. Conclusion

This study reviewed and concisely summarized the recent researches on the application of nanofluid in minichannel for heat transfer augmentation with emphasis on experimental and numerical works conducted with the following inferences made from the review:

- Nanofluid due to its higher surface to volume ratio can significantly improve heat transfer than the base fluid, and hybrid nanofluid formed from a combination of more than one nanofluids has better enhancement than the individual nanofluids.
- Thermal conductivity depends on size, material, and concentration of nanoparticles. Similarly, viscosity also depends on nanoparticles concentration. Addition of surfactant can reduce agglomeration of nanoparticles, but it can increase the viscosity of the nanofluid, hence it might affect the heat transfer enhancement.
- Thermophysical properties such as thermal conductivity, viscosity, material density, and specific heat capacity can be solved using classical theories, like Einstein, Maxwell, etc., however, these theories failed to describe thermal conductivity and viscosity of nanofluids, because those models considered only macro-sized particles.
- Two-phase models predict better results for convective heat transfer due to consideration of slip mechanism between nanoparticles and the base fluid, which is mostly neglected in single-phase approach, though contradictory results reduced the certainty of the results obtained using these approaches.
- Most of the researchers affirmed that use of nanofluid as an alternative to the conventional fluid can enhance the heat efficiency in heat exchangers and electronic devices in most cases by up to 50% thereby ensuring the system reliability.
- reduction of hydraulic diameter can effectively remove excess heat and improves the heat transfer coefficient (HTC), thus, a lot of methods were introduced by changing minichannel geometrical parameters, such as channel number, aspect ratio, cross-sections and path configurations; creating secondary flow, cavity, constriction along the passage and roughness of the surface.

Thus, it is recommended that, future works should be expected to dwell on modification of classical theories or new correlations needed to incorporate micro and nano-sized particles for determination of thermophysical properties, and determination of heat transfer mechanism of nanofluid in minichannel with emphasis on optimum enhancement of its thermophysical properties, as well as design of different shapes of minichannel heat sinks that are practicable and economically feasible.

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